

Optimal Experimental Design for Parameter Estimation in Column and Lysimeter Experiments

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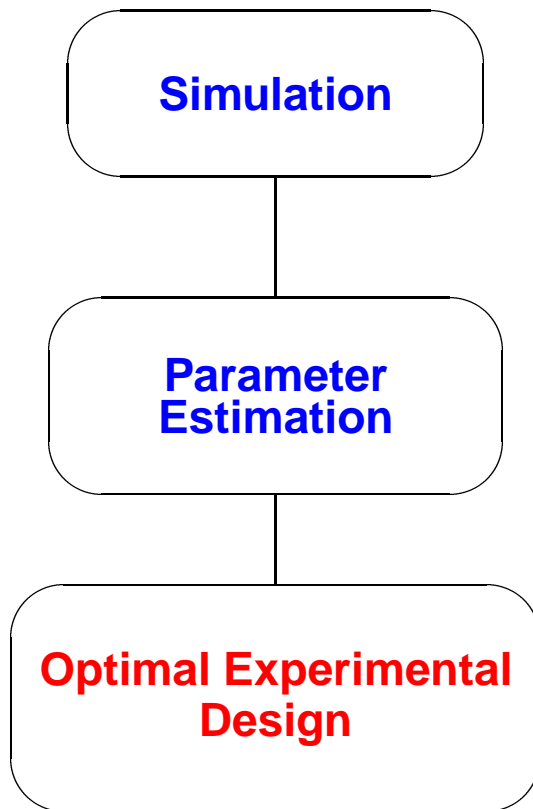
- Formulation of the inverse problem and its efficient solution
- Statistical quality of parameter estimates
- Formulation of the design problem as an optimal control problem
- Numerical solution of the optimization problem

Application: Design of Column Outflow Experiments

- Scenario 1: Optimization of experimental conditions
- Scenario 2: Simultaneous optimization of experimental conditions and sampling scheme

Why Optimal Experimental Design?

AIM: Reliable Simulation Models



Motivation

- For registration: Performance of many expensive column and lysimeter studies
- Substitution by computer simulations
⇒ enormous savings
- Determination of unknown parameters

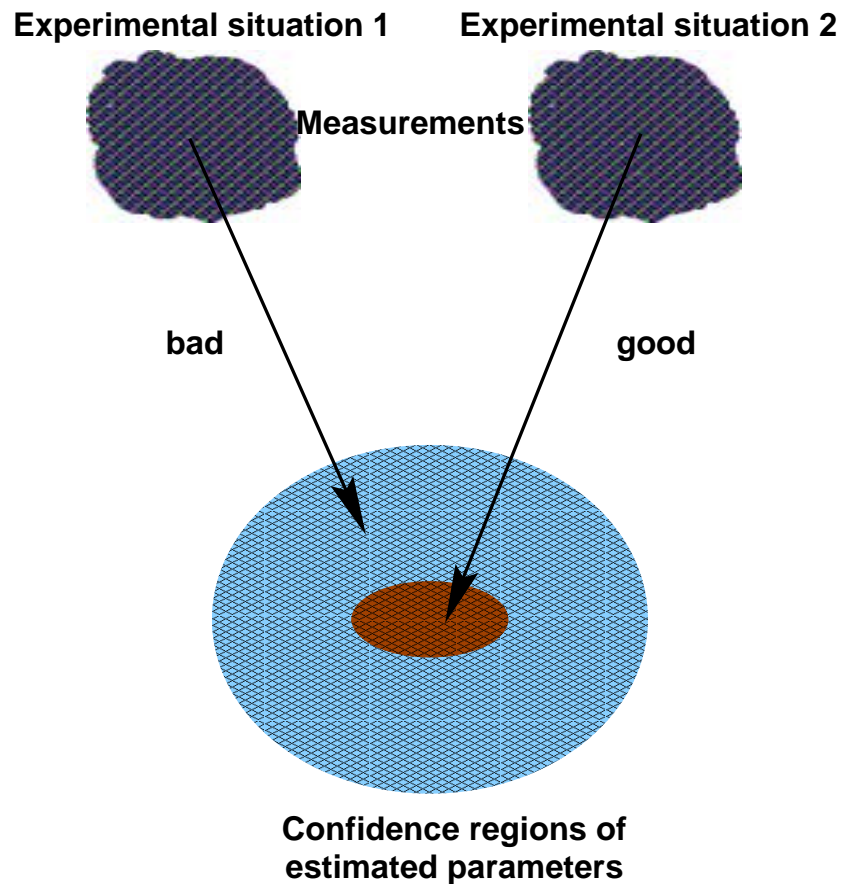
Problem

- Often unsuitable data for parameter estimation
⇒ ill-conditioned or singular problems

Remedy: “optimal” data

- optimal experimental conditions
- optimal sampling schemes

Optimal Experimental Design



- How inflow rates and/or input substance concentrations should be chosen?
- What, when and where measurements should be carried out?

Formulation of the Inverse Problem

Given: experimental data η_{kij} , ($k = \psi, \theta, c_l$), ($l = 1, \dots, n$), ($i = 1, \dots, m_1$), ($j = 1, \dots, m_2$)

$$\eta_{kij} = b_k(t_i, z_j, k(t_i, z_j), \mathbf{p}) + \varepsilon_{kij}, \quad \varepsilon_{kij} \sim N(0, \sigma_{kij}^2)$$

Aim: vector of parameters \mathbf{p} and a solution $k(t, z)$, such that

$$\begin{aligned} \min \|F(\psi, \theta, c_l; \mathbf{p})\|_2^2 &= \min \sum_{k=\psi, \theta, c_l} \sum_{i=1}^{m_1} \sum_{j=1}^{m_2} \sigma_{kij}^{-2} (\eta_{kij} - b_k(t_i, z_j, k(t_i, z_j), \mathbf{p}))^2 \\ C(\psi; \mathbf{p}) \frac{\partial \psi}{\partial t} &= \frac{\partial}{\partial z} (K(\psi; \mathbf{p}) \frac{\partial}{\partial z} (\psi - z)) + S_1(\psi; \mathbf{p}) \\ \frac{\partial \theta}{\partial t} &= \frac{\partial}{\partial z} (\bar{D}(\theta; \mathbf{p}) \frac{\partial \theta}{\partial z} - \bar{K}(\theta; \mathbf{p})) + S_2(\theta; \mathbf{p}) \\ \frac{\partial(\theta c_l)}{\partial t} + \frac{\partial(\rho S_l)}{\partial t} &= \frac{\partial}{\partial z} (\theta D_{h_l}(\theta; \mathbf{p}) \frac{\partial c_l}{\partial z}) - \frac{\partial}{\partial z} (q(\mathbf{p}) c_l) + Q_l(c_1, \dots, c_n; \mathbf{p}) \\ &+ \text{initial and boundary conditions} \end{aligned}$$

Efficient Solution of the Parameter Estimation Problem

- Discretization: Method of Lines

- Space: Finite Differences
- Time: Multiple Shooting

⇒ **large scale**, nonlinear, constrained least-squares problem

$$\begin{aligned} \min_p \|r_1(y(t_0; \mathbf{p}), \dots, y(t_f; \mathbf{p}), \mathbf{p})\|_2^2 &= \min_p \sum_{i,j} \frac{(\eta_{ij} - b_i(t_j, y(t_j; \mathbf{p}), \mathbf{p}))^2}{\sigma_{ij}^2} \\ r_2(y(t_0; \mathbf{p}), \dots, y(t_f; \mathbf{p}), \mathbf{p}) &= 0 \end{aligned}$$

- Reduced generalized Gauss Newton method

- very efficient generation of derivatives

⇒ **ECOFIT** (Dieses, Schlöder, Bock)

Statistical Quality of Parameter Estimates

Variance-Covariance Matrix

$$C(q, w, \hat{p}) = J(q, w, \hat{p})^+ \begin{pmatrix} I & 0 \\ 0 & 0 \end{pmatrix} J(q, w, \hat{p})^{+T}$$

- Experimental conditions: control functions q
- Sampling scheme: weights for measurement points w

⇒ Parameter estimation: q and w fixed

⇒ Optimal experimental design: \hat{p} fixed

$$C(q, w, \hat{p}) = J(q, w, \hat{p})^+ \begin{pmatrix} I & 0 \\ 0 & 0 \end{pmatrix} J(q, w, \hat{p})^{+T}$$

Optimal Experimental Design Problem

1. Choose an optimality criterion (A-,D-,E-Optimality)
here: A-Optimality: average variances of parameter estimates

$$\Phi_1(C) = \frac{1}{n} \text{trace}(C)$$

2. Define

- (a) Set of feasible experimental conditions E
- (b) Set of n feasible measurement points M

3. Determine

- (a) Optimal experimental conditions $q^* \in E$
- (b) Optimal sampling scheme, e.g. weights $w^* \in \{0, 1\}^n$

with

$$\Phi_1(C(q^*, w^*)) = \min_{q \in E, w \in \{0, 1\}^n} \Phi_1(C(q, w))$$

Nonlinear State-Constrained Optimal Control Problem

$$\min_{q,w} \Phi \left(C \left(J(y(p,q), p, q, w) \right) \right)$$

$$\dot{y} = f(t, y, p, q)$$

Control and state constraints:

$$c(y(t), q) \left\{ \begin{array}{l} = \\ \geq \end{array} \right\} 0$$

Interior-point conditions:

$$d(y(t_0; p, q, w) \dots, y(t_f; p, q), p, q, w) \left\{ \begin{array}{l} = \\ \geq \end{array} \right\} 0$$

Difficulty:

Objective function that implicitly depends on the Jacobian of the underlying parameter estimation problem in PDEs and ODEs.

Numerical Solution of the Optimization Problem

- **Direct Approach:** Parameterization of control functions (piecewise constant/linear)

⇒ finite dimensional nonlinear constrained optimization problem

$$\begin{aligned} \min_{\mathbf{v}} F(\mathbf{v}) \\ G(\mathbf{v}) = 0 \\ H(\mathbf{v}) \geq 0 \end{aligned}$$

\mathbf{v} : Parameterization of controls q and weights w .

⇒ solved by structured SQP-method

⇒ **VPLAN** (Körkel, Bauer, Bock, Schlöder, Sager, Rücker)

⇒ **ECOPLAN** (Dieses, Körkel, Schlöder, Bock)

Typical Column Outflow Experiment

Water transport: \implies 3 unknown parameters n, α, K_s

$$C(\psi) \frac{\partial \psi}{\partial t} = \frac{\partial}{\partial z} \left(K(\psi) \frac{\partial (\psi - z)}{\partial z} \right)$$

$$K(\psi) = K_s \frac{(1 - (\alpha|\psi|)^{n-1} (1 + (\alpha|\psi|^n)^{1/n-1})^2}{(1 + (\alpha|\psi|^n)^{1-1/n})^{\frac{1-1/n}{2}}}$$

$$C(\psi) = \alpha(n-1)(\theta_s - \theta_r)(\alpha|\psi|)^{n-1} (1 + (\alpha|\psi|^n)^{1/n-1})^{1/n-2}$$

- Initial condition: $\psi(0, z) = 670, \quad z \geq 0$
- Upper boundary condition:

$$q(t, 0) = -K(\psi(t, 0)) \left(\frac{\partial \psi(t, 0)}{\partial z} - 1 \right) \quad \text{control function}$$

- Lower boundary condition: $\frac{\partial \psi(t, L_e)}{\partial z} = 0, \quad t \geq 0$

Solute transport: \implies 3 unknown parameters k, b, D_m

$$\frac{\partial(\theta c)}{\partial t} = \frac{\partial(\theta D_h(\theta) \frac{\partial c}{\partial z})}{\partial z} - \frac{\partial(qc)}{\partial z} - kc$$

$$D_h(\theta) = \frac{0.0046e^{b\theta}}{\theta} + D_m$$

• Initial condition: $c(0, z) = 0, \quad z \geq 0$

• Upper boundary condition:

$$-D_h(\theta(t, 0)) \frac{\partial c(t, 0)}{\partial z} + \frac{q(t, 0)}{\theta(t, 0)} c(t, 0) = \frac{q(t, 0)}{\theta(t, 0)} c_0(t, 0)$$

• Lower boundary condition: $\frac{\partial c(t, L_e)}{\partial z} = 0, \quad t \geq 0$

\implies Coupled water and solute transport: 6 unknown parameters

Scenario 1: Optimization of Experimental Conditions

Experimental Conditions: 2 Control functions

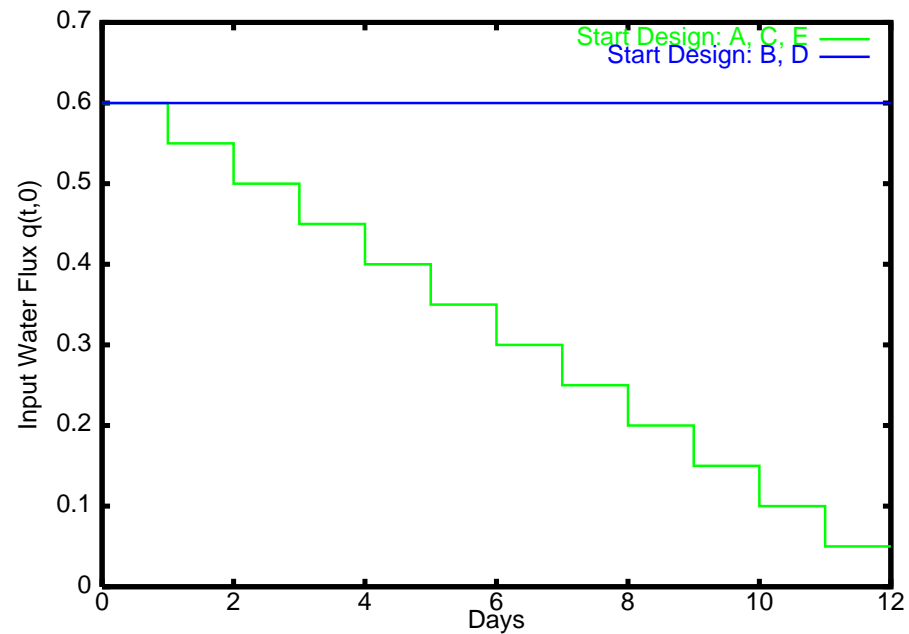
- Parameterization of the input water flux $q(t, 0)$
 - Changing in controls possible every 24 hours
 - Piecewise constant in the range of [0, 0.6]
- Parameterization of the substance input concentration $c_0(t, 0)$
 - Changing in controls possible every 24 hours
 - Piecewise constant in the range of [50,200]

Sampling Scheme: Fixed Measurements

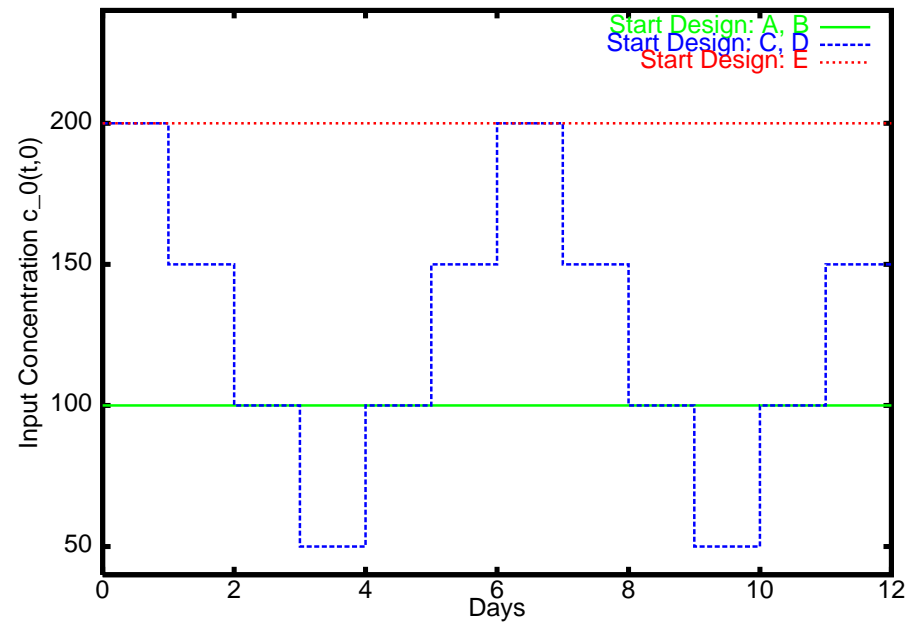
- 24 outflow measurements within 12 days: every 12 hours ($\sigma = 0.01$)
- 6 profile measurements ($\sigma = 0.1$)
 - At the end of the experiment ($T=12$ days)
 - Determination of concentration c in 6 depths.

Parameterized Start Designs

Input water flux $q(t,0)$



Substance input concentration $c_0(t,0)$



Quality of Start Designs: A-Criterion Values and Standard Deviations

Start Design A

A-Criterion = 3.8859

	scaled		standard deviation
n	1.0	±	0.1604
α	1.0	±	1.5968
K_s	1.0	±	3.3752
k	1.0	±	0.0124
b	1.0	±	3.0460
D_m	1.0	±	0.2644

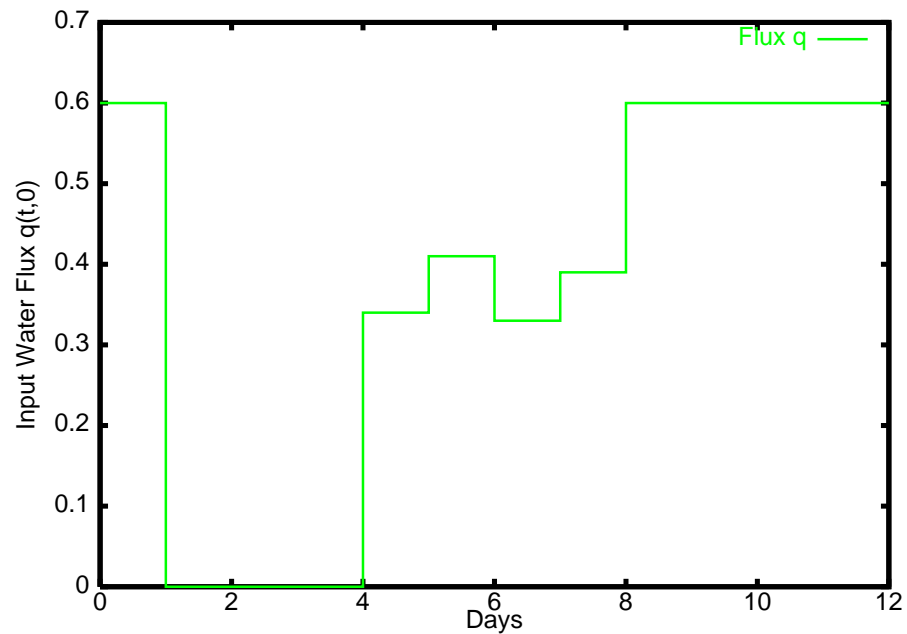
Start Design B

A-Criterion = 0.75

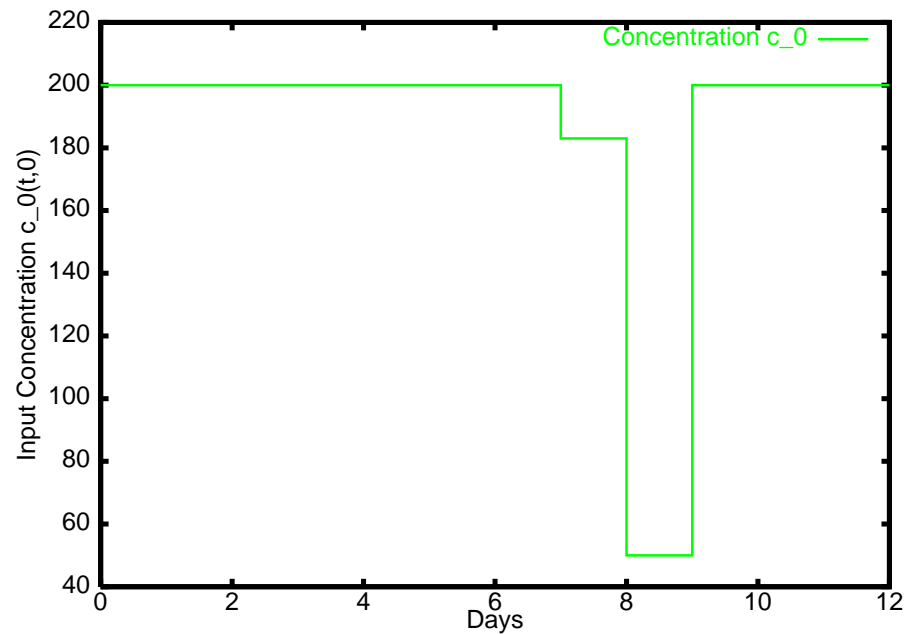
	scaled		standard deviation
n	1.0	±	0.0800
α	1.0	±	0.8600
K_s	1.0	±	1.6736
k	1.0	±	0.0083
b	1.0	±	0.9712
D_m	1.0	±	0.1033

Optimal Experimental Conditions

Input water flux $q(t,0)$



Substance input concentration $c_0(t,0)$



Comparison of Optimal Design with Start Designs A and B

		Optimal design	Start design A	Start design B
A-Criterion		0.0472	3.8859	0.750
n	1.0	± 0.0191	± 0.1604	± 0.0800
α	1.0	± 0.2438	± 1.5968	± 0.8600
K_s	1.0	± 0.4348	± 3.3751	± 1.6735
k	1.0	± 0.0086	± 0.0124	± 0.0083
b	1.0	± 0.1852	± 3.0460	± 0.9712
D_m	1.0	± 0.0108	± 0.2644	± 0.1032

Influence of Profile Measurements on the Designs

	Experiment 1	Experiment 2	Experiment 3
A-Criterion	0.0472	0.0749	0.0038
<i>n</i>	1.0 ± 0.0191	± 0.0283	± 0.0047
<i>α</i>	1.0 ± 0.2438	± 0.2850	± 0.0747
<i>K_s</i>	1.0 ± 0.4348	± 0.4735	± 0.1126
<i>k</i>	1.0 ± 0.0086	± 0.0121	± 0.0001
<i>b</i>	1.0 ± 0.1852	± 0.3764	± 0.0691
<i>D_m</i>	1.0 ± 0.0108	± 0.0351	± 0.0064

- Experiment 1: 24 outflow measurements ($\sigma=0.01$) + 6 profile measurements ($\sigma=0.1$)
- Experiment 2: ONLY 24 outflow measurements ($\sigma=0.01$)
- Experiment 3: 24 outflow measurements ($\sigma=0.01$) + 6 profile measurements ($\sigma=0.01$)

Scenario 2: Optimization of Experimental Conditions and Sampling Scheme

Experimental Conditions

- Control functions $q(t,0)$ and $c_0(t,0)$
- Start designs as in Scenario 1

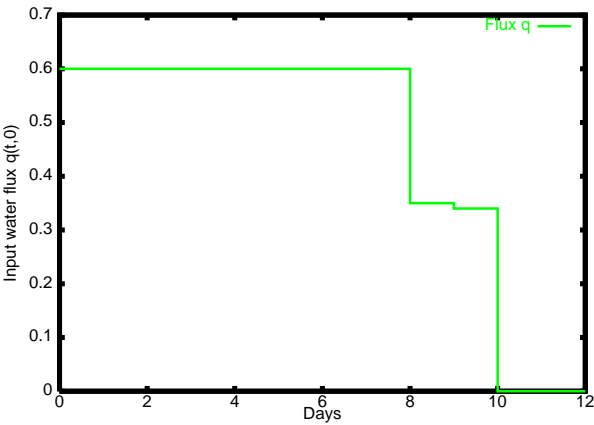
Sampling Scheme

- Outflow Data:
Measurements are feasible every 6 hours
⇒ Choose 24 measurements out of 48 feasible measurements
- Profile data:
fixed as in Scenario 1

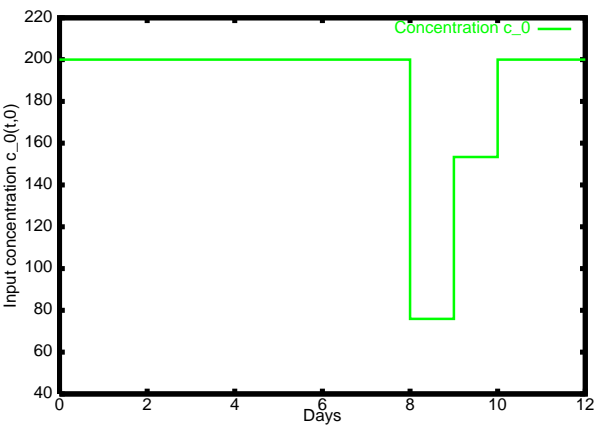
	Scen. 1	Scen. 2
A-Criterion	0.047	0.026
n	1.0 ± 0.0191	± 0.0215
α	1.0 ± 0.2438	± 0.2030
K_s	1.0 ± 0.4348	± 0.2872
k	1.0 ± 0.00857	± 0.0050
b	1.0 ± 0.1852	± 0.1876
D_m	1.0 ± 0.0108	± 0.0217

Optimal Experimental Conditions and Sampling Scheme

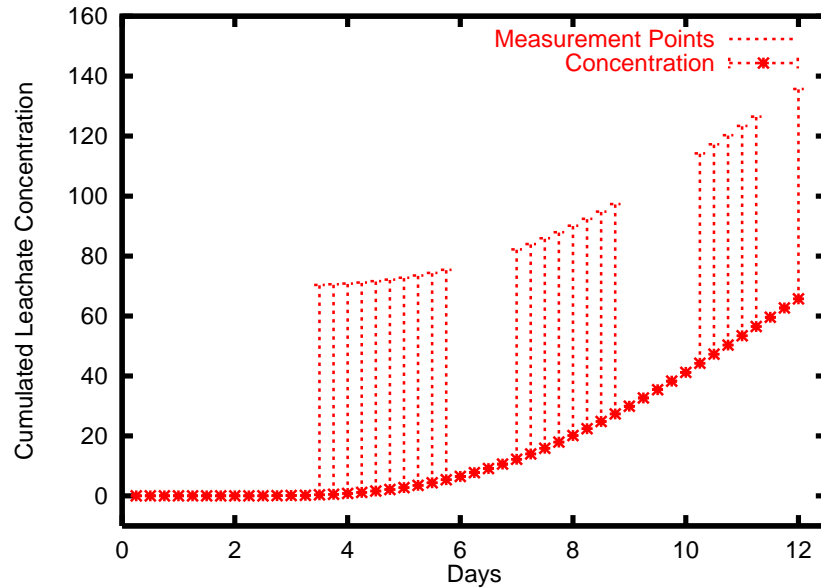
Input water flux $q(t, 0)$



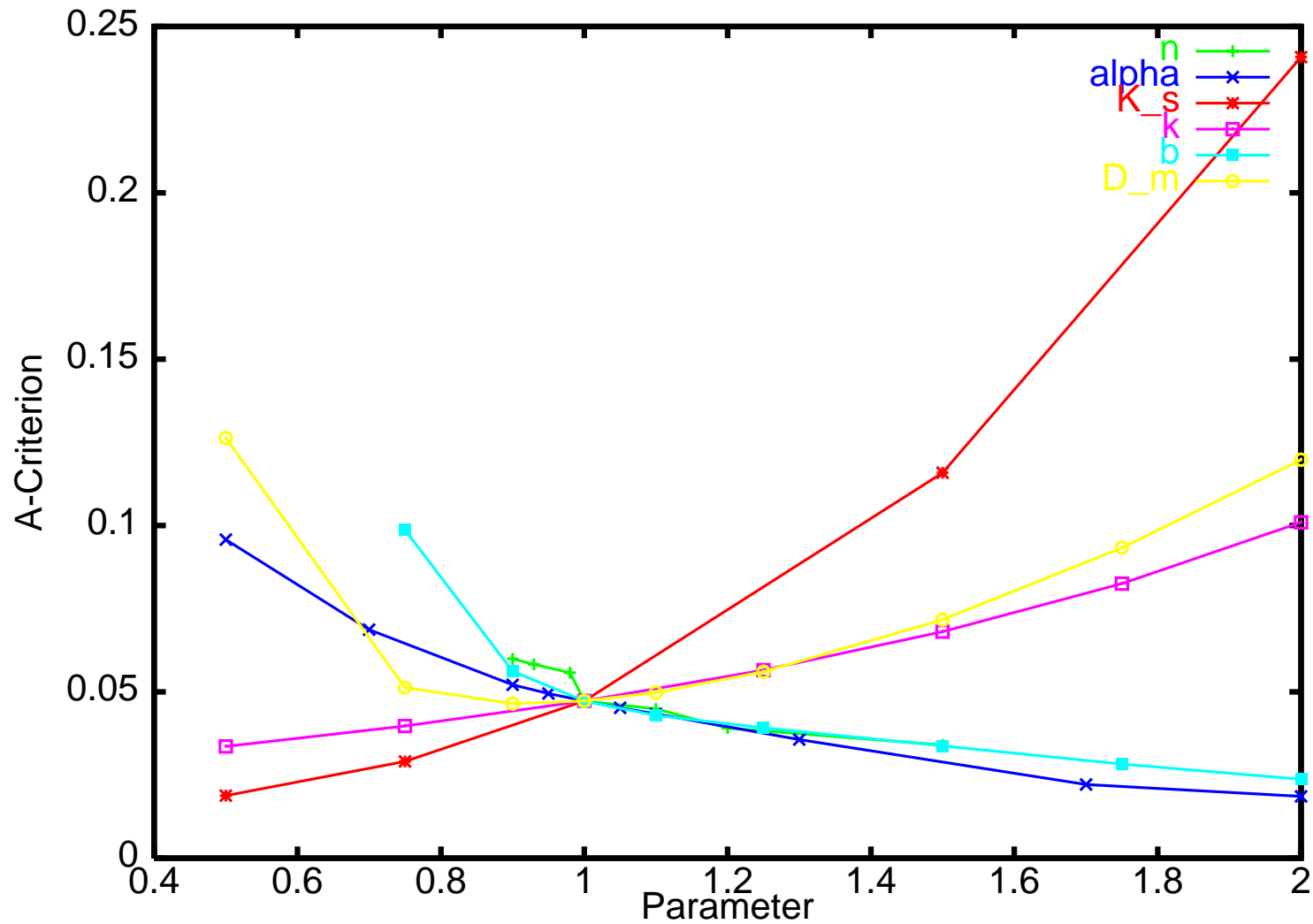
Input concentration $c_0(t, 0)$



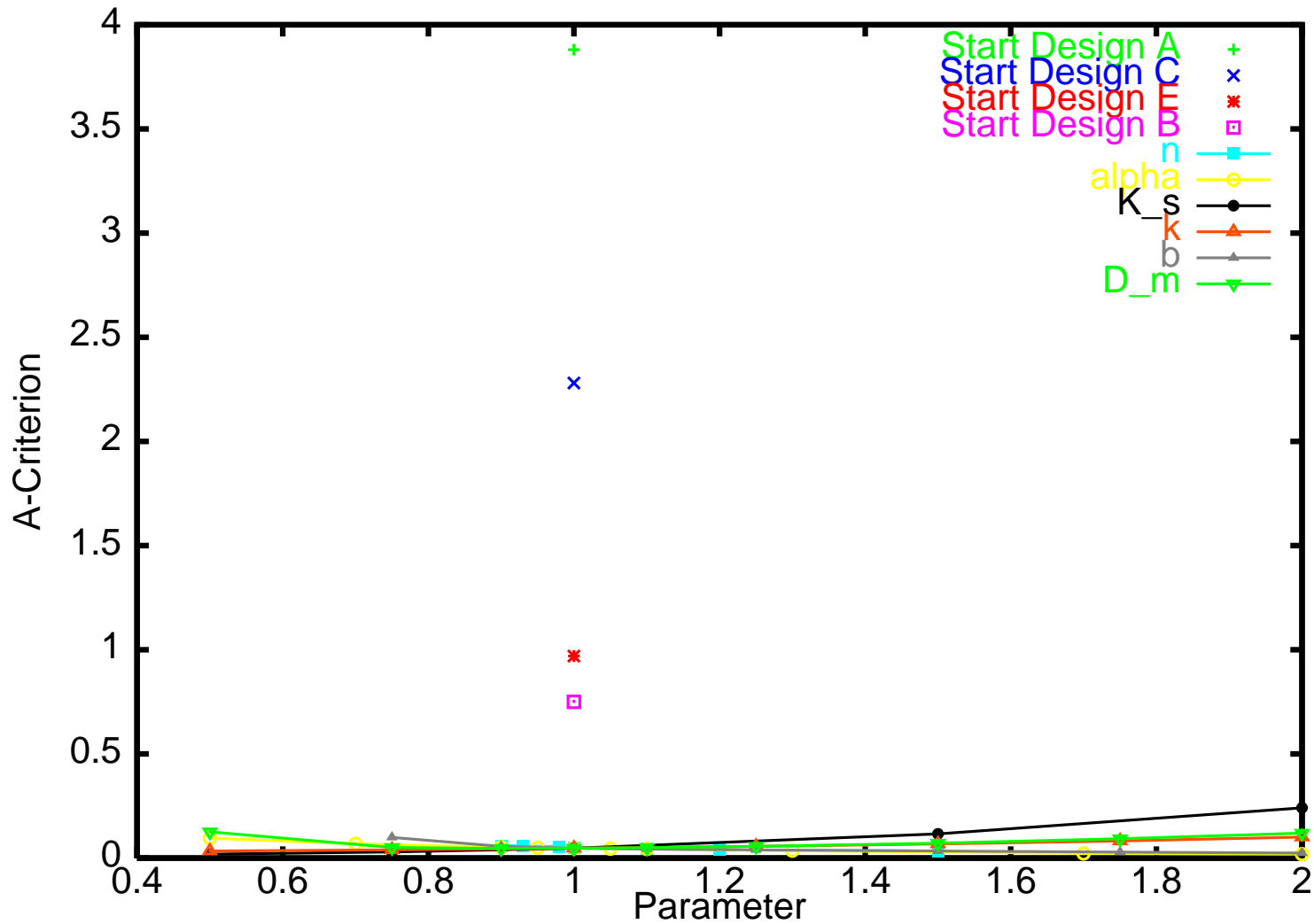
Allocation of Measurement Points



Parameter Sensitivity of Designs



Comparison: Start Designs - Optimal Design



Summary and Outlook

For transport and degradation processes of pesticides in soils we developed:

- Methods for parameter estimation \implies **ECOFIT**
- Methods for optimal experimental design \implies **ECOPLAN**

- Experiments on the basis of optimized designs
- General strategies for column and lysimeter experiments
 \implies Registration